

A meshless solution of two dimensional density-driven groundwater flow

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Abstract

The boundary element method (BEM) is a very useful method used for numerical models of groundwater flow. However, this method was aimed to solve problems in homogeneous domains and it presents even greater difficulties than the other numerical methods when coping with the nonhomogeneities which are so characteristic in the groundwater hydraulics. The meshless LBIE method is a very promising meshless scheme. This method is characterized as meshless since distributed nodal points, covering the domain, are employed. Nodal points can be randomly spread over the domain. Every node is surrounded by a simple surface (circle) centered at the collocation point and the boundary integral equation is written on this local boundary. The unknown variables, in the local sub-domains, are approximated by some of the interpolation methods to obtain a system of linear equations. Solving this system of equations leads to the numerical solution for the main problem. Several authors used the moving least squares (MLS) method as an interpolation method but nowadays the radial basis functions (RBF) interpolation is used instead. In this paper the combination of RBF and the dual reciprocity method is used to solve the time-dependent groundwater flow in heterogeneous domain combined with temperature transport which also influences the density and viscosity of groundwater.

Keywords: heat transfer, density driven flow, dual reciprocity, radial basis functions.

1 Introduction

The density driven groundwater flow occurs mainly in some environmental problems such as saltwater intrusion or leakage from landfills. We must solve this problem also when we study the geothermal problems. Although density driven



flow problems are mainly three-dimensional, they are often simulated by vertical 2D numerical models due to their very high computational costs.

The boundary element method and dual reciprocity method (DRM) are very useful methods used for numerical models of groundwater flow (see e.g. [1]). However, these method was mainly aimed to solve problems in homogeneous domains and it presents some difficulties when coping with the non homogeneities which are so characteristic of the groundwater hydraulics. The disadvantage can be overcome using some meshless scheme combined with BEM or DRM. The meshless LBIE method, introduced by Zhu et al. [2], is a very promising meshless scheme. This method is characterized as meshless since distributed nodal points, covering the domain, are employed. Nodal points are randomly spread over the domain. Every node is surrounded by a simple surface (circle) centered at the collocation point and the boundary integral equation is written on this local boundary. The unknown variables, in the local sub-domains, are approximated by some of the interpolation method to obtain a system of linear equations. Solving this system of equations leads to the numerical solution for the main problem. Zhu et al. [2] used the moving least squares (MLS) method as an interpolation method but nowadays the RBF interpolation is used instead (see e.g. [3]). In this paper the solution of coupled groundwater flow-heat transfer problem based on this RBIE method is presented.

2 Governing equations

A density-driven groundwater flow can be described by the following equation (see also [4])

$$\rho S \frac{\partial h}{\partial t} + \epsilon \frac{\partial \rho}{\partial t} + \nabla(\rho \vec{q}) = 0 \quad (1)$$

where h is the groundwater potential, ϵ is the porosity of porous medium, ρ is the density of solution and \vec{q} is the flux defined by

$$\mathbf{q} = -\mathbf{K} \left(\nabla h + \frac{\rho - \rho_0}{\rho_0} \nabla \vec{x} \right) \quad (2)$$

where \mathbf{K} is matrix of hydraulic conductivities and ρ_0 initial density of water. The differential equation of 2D groundwater flow with variable density is now expressed as

$$\frac{\partial}{\partial x} \left(\rho K_x \frac{\partial h}{\partial x} \right) + \frac{\partial}{\partial y} \left[\rho K_y \left(\frac{\partial h}{\partial y} + \frac{\rho - \rho_0}{\rho_0} \right) \right] = \epsilon \frac{\partial \rho}{\partial t} + \rho S \frac{\partial h}{\partial t} \quad (3)$$

where we denote K_x, K_y hydraulic conductivities [LT^{-1}] in direction x and y , respectively. Heat transfer in porous media can be described by the following



equation (see e.g. [5])

$$\frac{\partial}{\partial x_i} \left(K_{TB} \frac{\partial T}{\partial x_j} - q_i \rho_{LC} T \right) = \rho_{BC} \frac{\partial T}{\partial t} \quad (4)$$

where T is temperature, K_T is thermal conductivity, c is specific heat capacity. The subscripts L and B refer to liquid and bulk phases, respectively.

3 Dual reciprocity formulation

The Eq. (3) can be transformed to the following shape

$$\begin{aligned} \frac{\partial^2 h}{\partial x^2} + \frac{K_y}{K_x} \frac{\partial^2 h}{\partial y^2} &= \frac{\epsilon}{K_x \rho} \frac{\partial \rho}{\partial t} + \frac{S}{K_x} \frac{\partial h}{\partial t} - \frac{1}{\rho} \frac{\partial \rho}{\partial x} \frac{\partial h}{\partial x} - \\ &- \frac{K_y}{K_x \rho} \frac{\partial \rho}{\partial y} \frac{\partial h}{\partial y} - \frac{K_y}{K_x \rho \rho_0} \frac{\partial}{\partial y} (\rho^2 - \rho \rho_0) \end{aligned} \quad (5)$$

To solve Eq. (5) in the domain Ω with boundary Γ using the DRM we should use the following transformation of co-ordinates

$$\tilde{x} = x \quad \tilde{y} = y \sqrt{\frac{K_x}{K_y}} \quad (6)$$

and we get

$$\begin{aligned} \frac{\partial^2 h}{\partial \tilde{x}^2} + \frac{\partial^2 h}{\partial \tilde{y}^2} &= \frac{\epsilon}{K_x \rho} \frac{\partial \rho}{\partial t} + \frac{S}{K_x} \frac{\partial h}{\partial t} - \frac{1}{\rho} \frac{\partial \rho}{\partial \tilde{x}} \frac{\partial h}{\partial \tilde{x}} - \\ &- \frac{1}{\rho} \sqrt{\frac{K_y}{K_x}} \frac{\partial \rho}{\partial \tilde{y}} \frac{\partial h}{\partial \tilde{y}} - \frac{1}{\rho \rho_0} \sqrt{\frac{K_y}{K_x}} \frac{\partial}{\partial \tilde{y}} (\rho^2 - \rho \rho_0) \end{aligned} \quad (7)$$

Applying the Green integral formula to the left side of Eq. (7) we get the following integral form

$$c_k h_k + \int_{\Gamma} \frac{\partial u_{kj}^*}{\partial n} h_j d\Gamma - \int_{\Gamma} u_{kj}^* \frac{\partial h_j}{\partial n} d\Gamma - \int_{\Omega} u_{kj}^* b_j d\Omega = 0 \quad (8)$$

Here b_j is the value of the right side of Eq. (7) in point j and u_{kj}^* is the fundamental solution of Laplace equation. The constant c_k has value from 0 to 1 being 0.5 if the point k is placed on the smooth boundary. The DRM is used to transform the domain integral in Eq. (8) to equivalent boundary integrals (see [6]). The basic idea is to expand the term b_j using the approximation

$$b_j \cong \sum_{i=1}^{N_b + N_i} \alpha_i f_{ij} \quad (9)$$

where α_i is a set of initially unknown coefficients and f_{ij} are approximating functions. The approximation employs N_b nodes on the boundary Γ and N_i points



inside the domain Ω . The functions f_{ij} in Eq. (9) belongs to the family of radial basis function. The most often used functions are

$$f_{ij} = 1 + \sum_{m=1}^n r_{ij}^m \tag{10}$$

Now we can define the series of particular solutions \hat{h}_{ij} . These solutions and the approximating functions f_{ij} are linked through the equation

$$\frac{\partial^2 \hat{h}_{ij}}{\partial \tilde{x}^2} + \frac{\partial^2 \hat{h}_{ij}}{\partial \tilde{y}^2} = f_{ij} \tag{11}$$

Applying the Green’s formula to the Eq. (11) and using Eq. (9) we can transform Eq. (8) and get the boundary only integral formula

$$\begin{aligned} & c_k h_k + \int_{\Gamma} \frac{\partial u_{kj}^*}{\partial n} h_j d\Gamma - \int_{\Gamma} u_{kj}^* \frac{\partial h_j}{\partial n} d\Gamma = \\ & = \sum_{i=1}^{N_b+N_i} \alpha_i \left(c_k \hat{h}_{ki} + \int_{\Gamma} \frac{\partial u_{ki}^*}{\partial n} \hat{h}_{ij} d\Gamma - \int_{\Gamma} u_{ki}^* \frac{\partial \hat{h}_{ij}}{\partial n} d\Gamma \right) \end{aligned} \tag{12}$$

The discretized form of Eq. (12) for source point k can be written as

$$\begin{aligned} & c_k h_k + \sum_{j=1}^{N_b} H_{kj} h_j - \sum_{j=1}^{N_b} G_{kj} q_j = \\ & = \sum_{i=1}^{N_b+N_i} \alpha_i \left(c_k \hat{h}_{ki} + \sum_{j=1}^{N_b} H_{ki} \hat{h}_{ij} - \sum_{j=1}^{N_b} G_{ki} \hat{q}_{ij} \right) \end{aligned} \tag{13}$$

where H_{kj} and G_{kj} are matrices obtained from the integrations of q^* and u^* at each boundary element. The unknown coefficients α_i can be determined from Eq. (9) as

$$\alpha_i = \sum_{j=1}^{N_b+N_i} F_{ij}^{-1} b_j \tag{14}$$

where F_{ij}^{-1} are members of the inverse matrix of values of function f_{ij} .

4 Radial basis functions interpolation

Radial basis functions (RBF) are initially known as a powerful tool for approximating multivariate functions on a scattered data. Due to their mesh-free nature RBF have received an increasing attention for solving partial differential equations (PDE) of different kinds. The first trial of such exploration was made by Kansa [7]. Full exploitation of the RBF method was constrained by the progressive

ill-conditioned coefficient matrix as the number of nodes increases. To remove this difficulty, Shu et al. (see [8]) suggested using the local RBF method in which the approximation is formed by using only several local supporting points. The unknown function U is approximated in a sub-domain which forms the neighborhood or support of a reference point i by weighted sum of multiquadric functions and polynomials

$$U(x_i, y_i) = \sum_{j=1}^n \lambda_j R(r_{ij}) + \sum_{j=1}^m \chi_j p_j(x_i, y_i) \quad (15)$$

where λ_j and χ_j are weights, $R(r_{ij})$ are the RBF basis functions, and p_j is a basis for polynomial space with degree $m - 1$, m is the order of R and n is a number of field nodes in the neighborhood of a reference point. Multiquadric functions are one of the most popular radial functions used for this purpose and they are defined as

$$R(r_{ij}) = \sqrt{r_{ij}^2 + \epsilon^2} \quad (16)$$

where r_{ij} is a distance between points i and j and ϵ is a so-called shape factor of multiquadric function. Coefficients λ_j , χ_j in Eq. (15) can be determined by enforcing Eq. (15) to be satisfied at these N_i nodes surrounding the point of interest. This leads to n linear equations, one for each node. The matrix form of these equations can be expressed as

$$\mathbf{U} = \mathbf{R}\lambda + \mathbf{P}\chi \quad (17)$$

where $\mathbf{U} = [U_1, U_2, \dots, U_{N_i}]$ is a vector of function values in all supporting nodes. However there are $n + m$ variables in this equation. The additional m equations can be added using the following m constraint conditions

$$\sum_{i=1}^n p_j(x_i, y_i) \lambda_i = 0, \quad j = 1 \dots m \quad (18)$$

Combining Eqs.(17) and (18) yields the following set of equations in the matrix form

$$\mathbf{u} = \mathbf{A}\mathbf{a} \quad (19)$$

where we denoted

$$\mathbf{A} = \begin{bmatrix} \mathbf{R} & \mathbf{p} \\ \mathbf{p}^T & \mathbf{0} \end{bmatrix}, \quad \mathbf{a} = \begin{Bmatrix} \lambda \\ \chi \end{Bmatrix}, \quad \mathbf{u} = \begin{Bmatrix} \mathbf{U} \\ \mathbf{0} \end{Bmatrix} \quad (20)$$

The order m of multiquadric functions is equal to one and, therefore, we need one additional condition to make the interpolation problem well-posed. This



condition is

$$\sum_{j=1}^n \lambda_j = 0 \tag{21}$$

Solving Eq. (19) we get

$$\mathbf{a} = \mathbf{A}^{-1}\mathbf{u} \tag{22}$$

Eq. (15) can be now written as (see e.g. [9])

$$U(x_i, y_i) = [\mathbf{R}^T(x_i, y_i) \mathbf{p}^T(x_i, y_i)]\mathbf{a} = [\mathbf{R}^T(x_i, y_i) \mathbf{p}^T(x_i, y_i)]\mathbf{A}^{-1}\mathbf{u} \tag{23}$$

The first n members of the product $[\mathbf{R}^T(x_i, y_i) \mathbf{p}^T(x_i, y_i)]\mathbf{A}^{-1}$ create set of RBF shape functions ϕ_j and Eq. (23) can be rewritten as

$$U(x_i, y_i) = \sum_{j=1}^n \phi_j U_j \tag{24}$$

This formula is used to develop the meshless local DRM in the next section.

5 Meshless local DRM formulation

In this section we follow the principle of RBIEM (see [3]). The area of interest Ω is covered by single nodes on the global boundary Γ and also inside the area (see Fig. 1). The local network of 16 elements was created around every node. This simplifies the generation of local boundaries and evaluation of integrals. Next four virtual internal points was added to every network (see Fig. 2) because the solution is usually more accurate (see [6]). The values of potential and its derivatives in

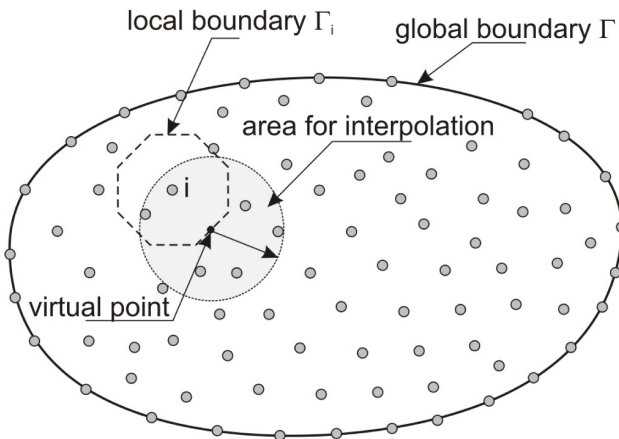


Figure 1: Nodes in the global area.

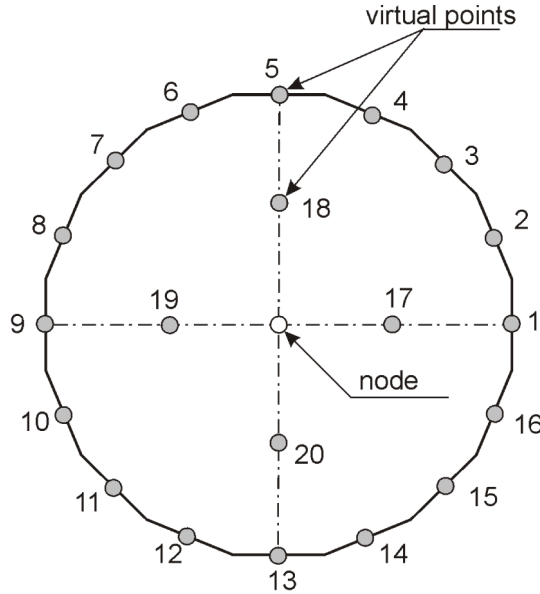


Figure 2: Local network.

x and y directions in node k can be computed from values of potentials and derivatives in virtual points using Eq. (9) as

$$h_k = \sum_{j=1}^{N_{vb}} G_{ij} q_{xj} n_x + \sum_{j=1}^{N_{vb}} G_{ij} q_{yj} n_y - \sum_{j=1}^{N_{vb}} H_{ij} h_j + \quad (25)$$

$$+ \sum_{k=1}^{N_{vb}+N_{vi}} \left\{ \alpha_k \left(c_i \hat{h}_{ik} + \sum_{j=1}^{N_{vb}} H_{ik} \hat{h}_{kj} - \sum_{j=1}^{N_{vb}} G_{ik} \hat{q}_{kj} \right) \right\}$$

$$\frac{\partial h_k}{\partial x} = \sum_{j=1}^{N_{vb}} \frac{\partial G_{ij}}{\partial x} q_{xj} n_x + \sum_{j=1}^{N_{vb}} \frac{\partial G_{ij}}{\partial x} q_{yj} n_y - \sum_{j=1}^{N_{vb}} \frac{\partial H_{ij}}{\partial x} h_j + \quad (26)$$

$$+ \sum_{k=1}^{N_{vb}+N_{vi}} \left\{ \alpha_k \left(\frac{\partial \hat{h}_{ik}}{\partial x} + \sum_{j=1}^{N_{vb}} \frac{\partial H_{ik}}{\partial x} \hat{h}_{kj} - \sum_{j=1}^{N_{vb}} \frac{\partial G_{ik}}{\partial x} \hat{q}_{kj} \right) \right\}$$

where N_{vb} is the number of virtual boundary points, N_{vi} is the number of virtual internal points, h_j are the values of potential in virtual points, q_{xj} , q_{yj} are the derivatives in boundary virtual points in x and y directions and n_x , n_y are the directional cosines of outer normal to virtual boundary, respectively. The derivative in direction y is computed according similar formula to Eq. (26). Values

of potential and its derivatives can be approximated using RBF interpolation according Eq. (24) and we get

$$\begin{aligned}
 h_k = & \sum_{j=1}^{N_{vb}} G_{ij} n_x \sum_{m=1}^n \phi_m q_{xm} + \sum_{j=1}^{N_{vb}} G_{ij} n_y \sum_{m=1}^n \phi_m q_{ym} - \quad (27) \\
 & - \sum_{j=1}^{N_{vb}} H_{ij} \sum_{m=1}^n \phi_m h_m + \\
 & + \sum_{k=1}^{N_{vb}+N_{vi}} \left\{ \alpha_k \left(c_i \hat{\Phi}_{ik} + \sum_{j=1}^{N_{vb}} H_{ik} \hat{\Phi}_{kj} - \sum_{j=1}^{N_{vb}} G_{ik} \hat{q}_{kj} \right) \right\}
 \end{aligned}$$

$$\begin{aligned}
 \frac{\partial h_k}{\partial x} = & \sum_{j=1}^{N_{vb}} \frac{\partial G_{ij}}{\partial x} n_x \sum_{m=1}^n \phi_m q_{xm} + \sum_{j=1}^{N_{vb}} \frac{\partial G_{ij}}{\partial x} n_y \sum_{m=1}^n \phi_m q_{ym} - \quad (28) \\
 & - \sum_{j=1}^{N_{vb}} \frac{\partial H_{ij}}{\partial x} \sum_{m=1}^n \phi_m h_m + \\
 & + \sum_{k=1}^{N_{vb}+N_{vi}} \left\{ \alpha_k \left(\frac{\partial \hat{h}_{ik}}{\partial x} + \sum_{j=1}^{N_{vb}} \frac{\partial H_{ik}}{\partial x} \hat{h}_{kj} - \sum_{j=1}^{N_{vb}} \frac{\partial G_{ik}}{\partial x} \hat{q}_{kj} \right) \right\}
 \end{aligned}$$

where h_m , q_{xm} , and q_{ym} are values of potential and derivatives in directions x and y in supporting nodes in the neighbourhood of corresponding virtual points.

Coefficients α_k is defined by Eq. (14). The backward difference is used to approximate the time derivatives of potential on the right side of Eq. (4) and we get the resulting recurrent system of equations to solve potential and its derivatives in every node. Equations of heat transfer are solved using the same RBIE method and also the similar algorithms as the potential flow.

Equations of flow and heat transfer are then coupled by the equations of state which gives the fluid density and viscosity as functions of temperature. The coupling scheme was realized by the sequential-iterative approach using the modified Pickard algorithm:

- Step1: Solution of the transfer equations
- Step2: Update fluid flow properties ρ , μ , K_x , K_y
- Step3: Solution of potential flow
- Step4: Compute velocities of flow
- Step5: Test the convergence of the process

This modified scheme converges much faster then the classical Pickard algorithm (see [10]).



6 Numerical example

The RBIEM model has been verified with the Elder problem (see [5]) of free geothermal convection. The 2D domain is vertically oriented rectangular area filled with a homogeneous isotropic porous medium (see Fig. 3). It is a free convection problem where fluid flow is driven purely by fluid density differences. The elevated temperature of 20°C decreases water density and creates a potentially unstable situation where denser fluid overlies less dense fluid which leads to upwelling of warm water and to the formation of thermal fingering. In homogeneous isotropic media, the onset of free geothermal convection can be determined by the value of Rayleigh number Ra (see e.g. [5]). This number is the ratio between buoyancy forces driving free convection and conductive forces. The dimensionless thermal Rayleigh number can be defined as

$$Ra = \frac{KHc_L\Delta\rho L}{K_T} \quad (29)$$

where K is the hydraulic conductivity, H is the height of the model domain, c_L is the specific heat of the liquid, K_T is the thermal conductivity, and $\Delta\rho$ is the fluid density difference between the top and the bottom of the domain. The minimum value of the critical Rayleigh number $Ra_{cr} = 4\pi^2$. It is valid if and only if the aspect ratio of the domain $a = L/H$ is an integer value (see [11]). According to theory, simulations with $Ra < Ra_{cr}$ are conductive, whereas systems with $Ra > Ra_{cr}$ exhibit convective and unstable flow.

The solved problem has the aspect ratio $a = L/H = 2$ and therefore the critical Rayleigh number is $Ra_{cr} = 4\pi^2 = 39.478$. The coefficients, used in the solution

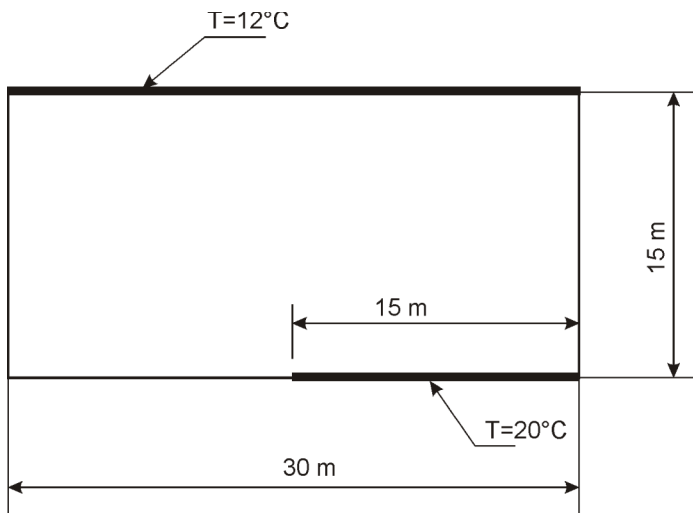


Figure 3: Elder problem.

Table 1: Parameters of the solved problem.

Quantity	Value	Unit
Porosity	0.1	—
Hydraulic conductivity	1.21E-04	ms^{-1}
Bulk thermal conductivity	1.49	$Wm^{-1}K^{-1}$
Specific heat capacity	4186	$Jkg^{-1}K^{-1}$
Initial temperature	12	$^{\circ}C$

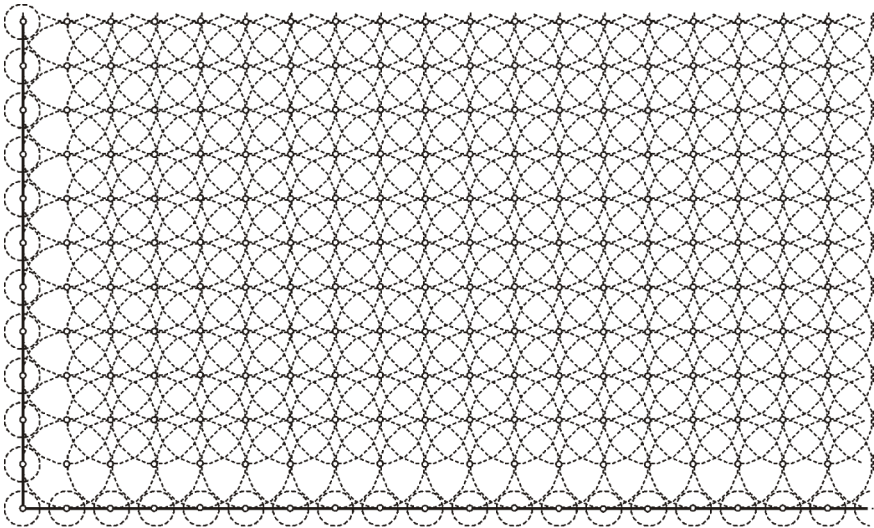


Figure 4: Detail of virtual network.

of the problem, are presented in Tab.1. The Rayleigh number computed for this problem is $Ra = 6.612 < Ra_{cr}$ and the problem is conductive and unstable flow should not occur. The domain is covered by 496 regularly distributed nodes and virtual networks were created around all node (see Fig. 4). The time step was 0.1 day. Fig. 5 shows the computed velocity field in 20 days and the increasing roll can be seen at the left part of the domain. The temperature distribution is presented in the form of isotherms at Fig. 6.

7 Conclusions

The possibility of RBIEM meshless method for modeling the density driven flow is presented in this paper. The research is at the beginning and the following study should be focused on the convective unstable situations models and on



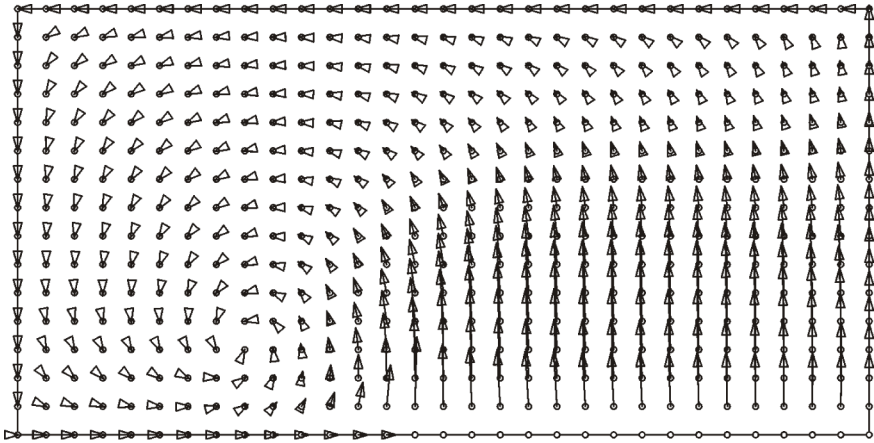


Figure 5: Resulting velocity field.

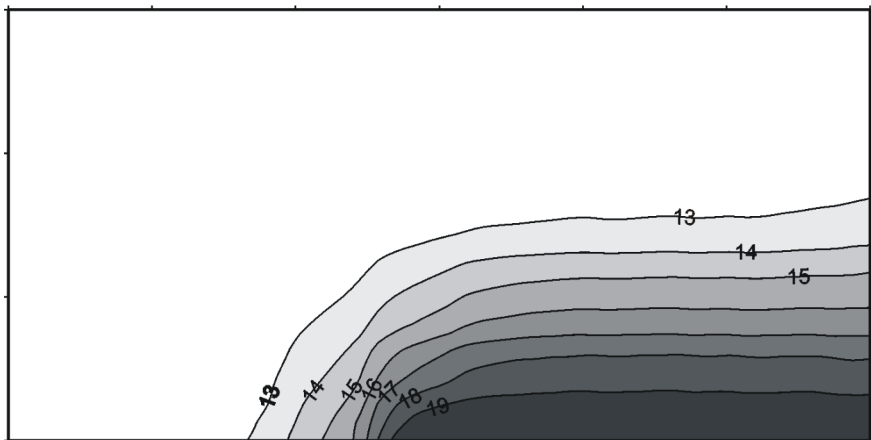


Figure 6: Isotherms.

the modification of the existing algorithms to enable distributed processing. It is necessary to choose suitable tools which give us ability to parallel solving of very large network systems which usually exist in practical solutions.

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